



Applying international experience for the dismantling of Chooz A SGs

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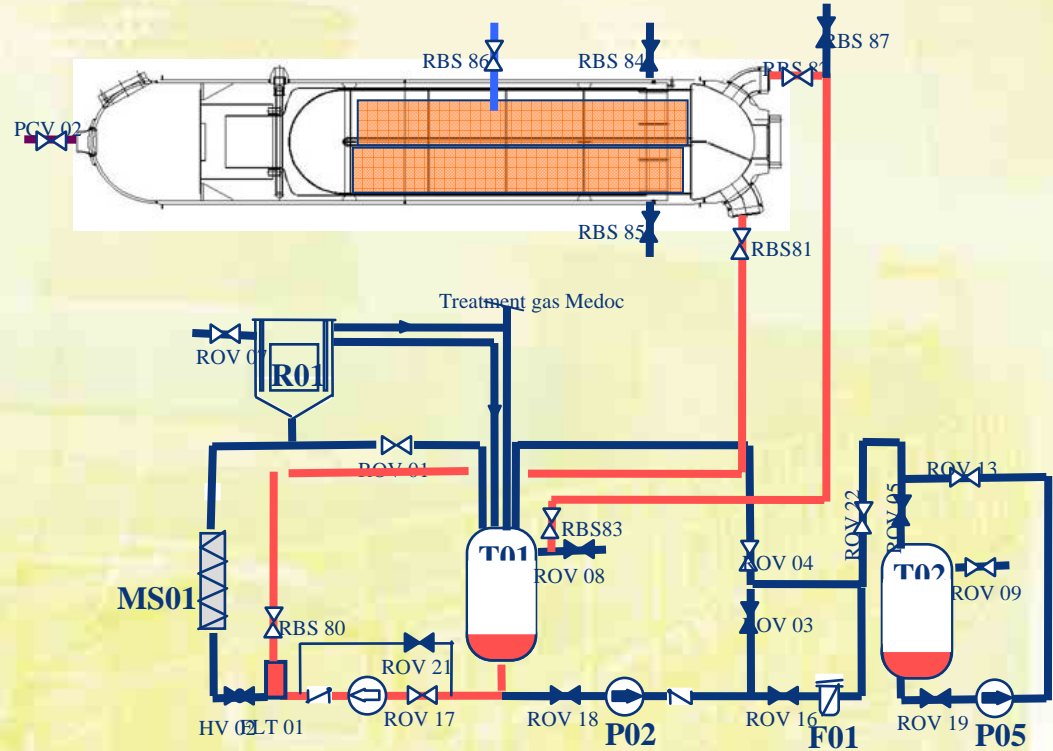
BR3 experience (Belgium)

- **Chemical decontamination**

 - ❖ **High Decontamination Factor (1000)**

 - MEDOC process

- **Free release after melting**



US experience regarding SG dismantling



- One piece disposal at a LLW repository after decontamination



Barnwell

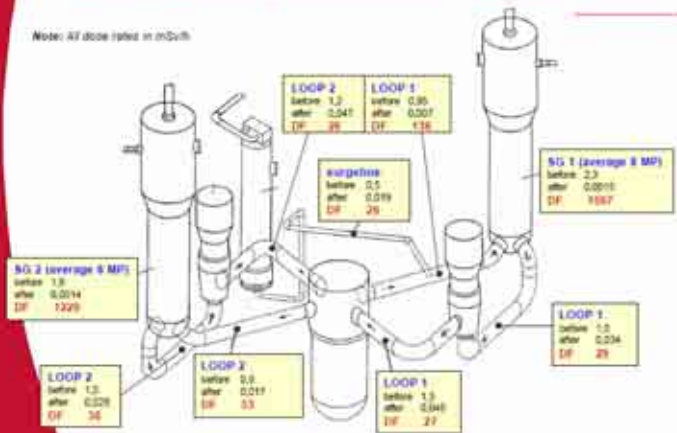


SG dismantling in Germany (Obrigheim)



Dose Rates and Deconactors – primary system

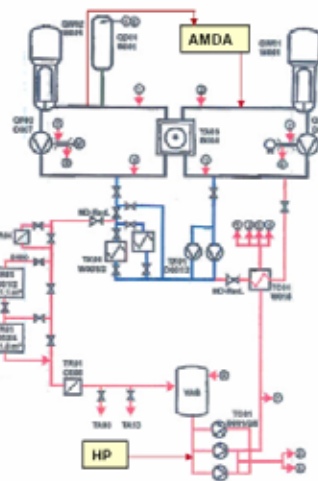
Note: All dose rates in mSv/h



Principle flow path

Decon Area:

- primary circuit (incl. RPV)
- RHR (TK01)
- VCS (TC01)
- RWCU (TR01)
(optional, not included in decon area)



System Volume	160 m ³ (42,267 gal)	
Surface	~ 8100 m ² (78200 ft ²)	approx. 6000 m ² (Incoloy 800)
		approx. 2100 m ² (austenitic steel)

HP Injection of Permanganic acid using NPP chemical injection system

- Full Scope Decontamination prior to dismantling

❖ HP CORD D UV

SG dismantling in Germany (Stade)

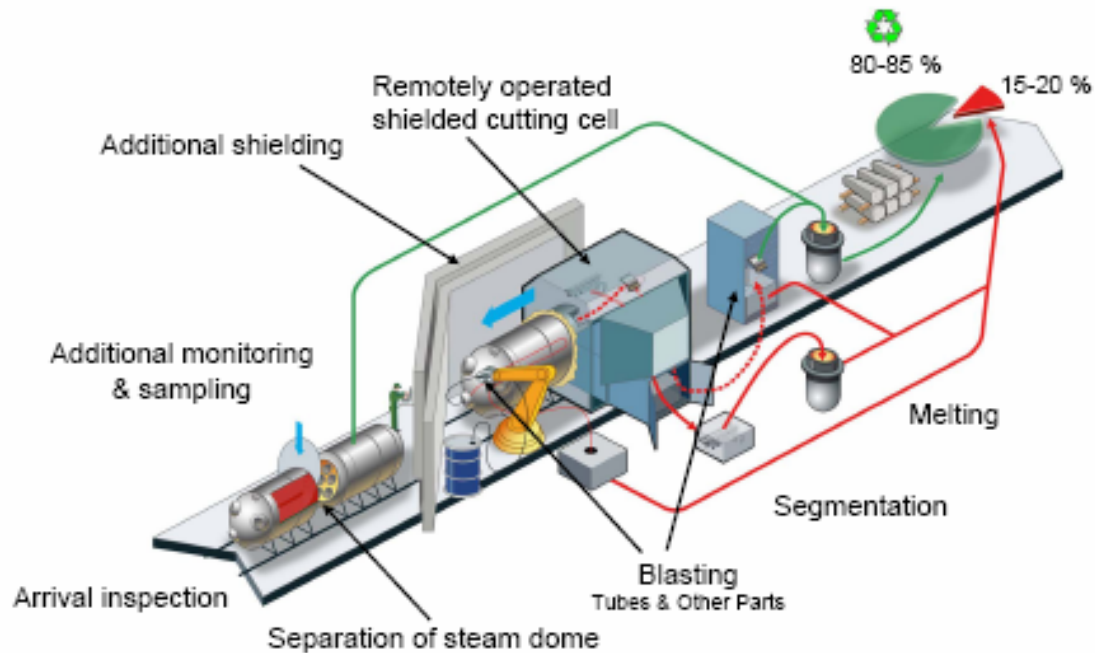


Stade SGs transported in 2007 to
Studsvik's facility for melting



Segmentation and melting at Studsvik's facility

Steam Generator Technical Concept



Studsvik





Context in France regarding WM

- Free release not allowed
- A VLLW repository is available
 - ❖ Waste disposal cost much lower than disposal cost at the LLW repository





Chooz A SGs dismantling

● Selected scenario

❖ Decontamination with a high Decontamination Factor

- Waste Decategorisation from LLW to VLLW (disposal cost reduction)

❖ One piece disposal

- Save time and exposure for the workers (no segmentation)
- Less release and secondary waste
- Less transportation
- Optimises the volume needed for disposal

● Issues to be solved

❖ SGs acceptance at the VLLW repository

❖ Secondary waste conditioning

- Depending on the decontamination process





Selection of the decontamination process

- **Open tender**
 - ❖ **No decontamination process prescribed**
 - ❖ **Objective : meet the criteria for VLLW category**
- **Contract award**
 - **Technical Criteria**
 - Demonstrate the efficiency of the decontamination process on samples
 - **Financial criteria**
 - Total cost for EDF (including secondary waste processing and disposal)
- **Drivers governing the selection by the contractor of the decontamination process**
 - ❖ **Secondary waste conditioning**
 - ❖ **Liquid release**
 - ❖ **Industrial experience**



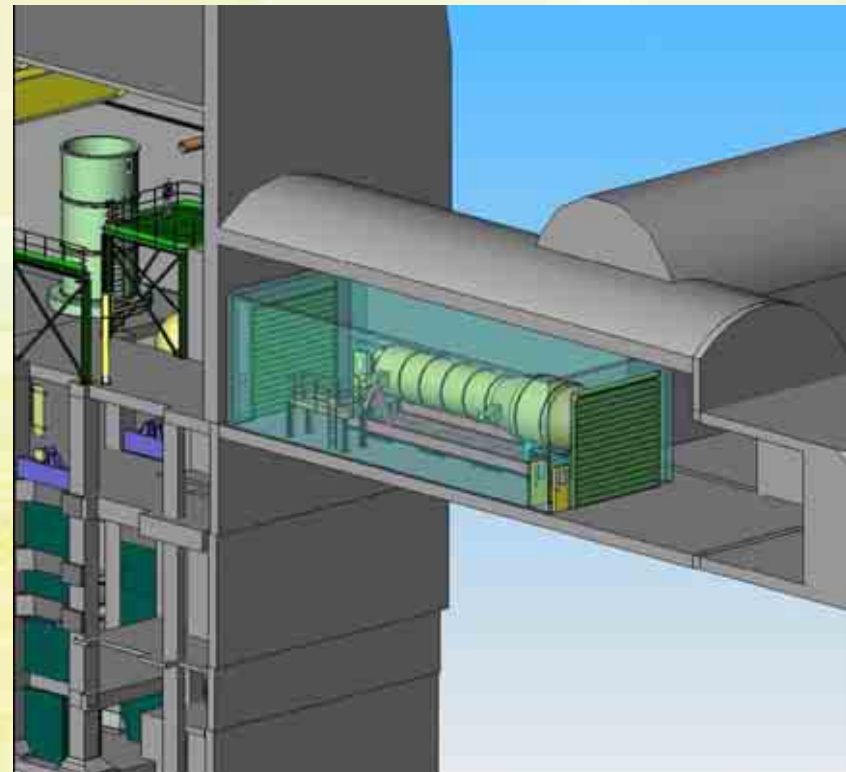
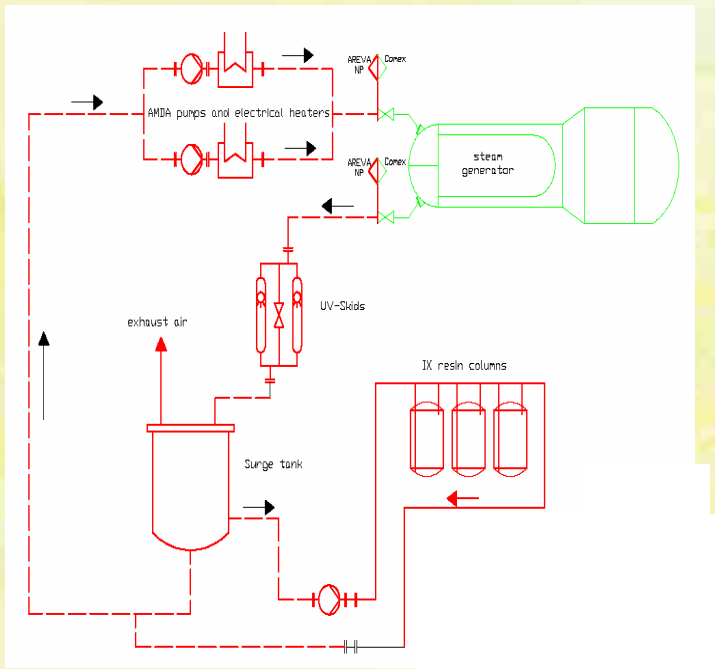


SG decontamination at Chooz A

- Chemical decontamination with a high decontamination factor

❖ HP CORD D UV

- One piece removal





Current situation

- **Contract awarded**
 - ❖ Detailed Design in progress
 - ❖ SG Decontamination planned in July 2010
 - ❖ Efficiency of the decontamination process to be demonstrated on really contaminated samples (planned in April 2009)
- **Issues still to be solved**
 - ❖ **SGs acceptance at the VLLW repository (under investigation by ANDRA)**
 - Development of a dedicated cell might be necessary (with heavy payloads handling tools)





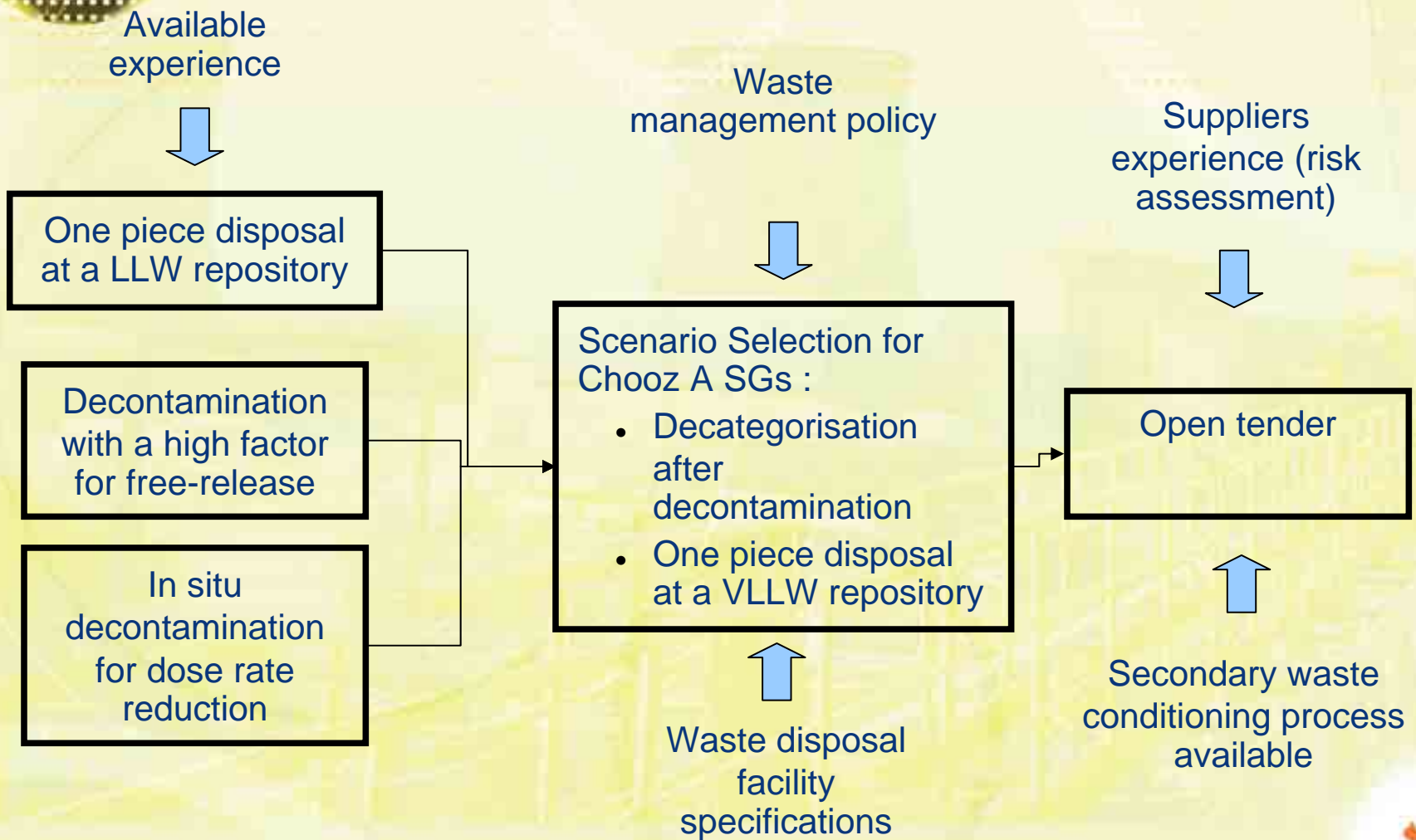
Conclusions

- **A simple Copy of BR3 experience was not possible**
 - ❖ **No free release**
 - ❖ **Decontamination process considered as not fully industrial by some suppliers (risk)**
 - ❖ **Secondary waste conditioning to be developed in France**
- **Chooz A SGs dismantling presents some residual risks**
 - ❖ **Efficiency of the decontamination process. Chooz A is still a first of its kind :**
 - **CORD UV never used for waste decategorisation**
 - ❖ **Acceptance at the VLLW repository**
 - **Alternative solutions to be considered**





Drivers governing Chooz A SGs dismantling





Reference

- **For similar experience regarding Reactor Pressure Vessel refer to :**

- **❖ WM 2009 – session 18**

- « International Cooperation for the Dismantling of Chooz A Reactor Pressure Vessel » - 9087 – JJ Grenouillet - EDF